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(54) **Cross-catalyzed phenol-resorcinol adhesive for lignocellulosic bonding and method of manufacture**

Kreuzkatalysierter Phenol-Resorcinklebstoff zum Kleben von Lignocellulosehaltigem Material und Verfahren zur Herstellung

Adhésif à catalyse croisée à base de résines phénoliques et résorcinoliques pour le collage de matériaux lignocellulosiques et procédé de fabrication

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(C-0825), 18 April 1991 & JP-A-03 031384 (AICA
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• **CHEMICAL ABSTRACTS**, vol. 78, no. 14, 9 April
1973 Columbus, Ohio, US; abstract no. 85338,
ZABRODKIN ET ALL. 'Adhesive composition'
page 40; & SU-A-355 195 (CENTRAL SCIENTIFIC
RESEARCH INSTITUTE OF PLYWOOD)

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Description

BACKGROUND OF THE INVENTION

1. Field of the Invention

[0001] This invention relates to an adhesive in two parts. The two parts are mixed together immediately prior to use. Part One is a stable aqueous alkaline phenolic resole resin solution containing a methylene donor. Part Two is a stable resorcinolic precondensate resin having a shortage of formaldehyde which optionally contains a catalyst for curing the resole resin. Each part exhibits viscosity stability of the respective resin similar to that without the methylene donor or catalyst until the two parts are mixed. On mixing, the methylene donor of Part One reacts with the resorcinolic resin of Part Two and the catalyst in Part Two reacts with the phenolic resole resin of Part One to cause adhesive gelation and cure of the resins. The adhesive is particularly useful for the manufacture of lignocellulosic panels such as strandboard.

2. Description of the Prior Art

[0002] Aqueous alkaline monohydroxylic phenolic resole resins are used in the structural board industry as durable binders to produce panel products intended for limited exterior use. Such resins have long been plagued with some drawbacks including a relatively long curing time and sensitivity to high moisture levels. Adhesive improvements in recent years have shortened curing times and reduced moisture sensitivity, but advances in these areas are still desirable. The introduction of polymeric isocyanate (polymeric methylene diisocyanate, or PMDI) as a binder for structural boards offers a new performance benchmark for phenolic resole resins. PMDI is a very fast curing adhesive that is relatively unaffected by wood moisture in the normal range encountered in a panel manufacturing plant. PMDI is very expensive, though, and questions are being raised about worker health concerns in plants using the adhesive.

[0003] The use of phenolic resole resin curing catalysts are known, e.g., such as those described in US-A-4,831,067 of 5/16/89 to Lemon et al; and US-A-4,961,795 of 10/9/90 to Detlefsen and Phillips. The above mentioned Detlefsen and Phillips patent is also concerned with methods for accelerating the cure of phenolic resole resins in the manufacture of lignocellulosic panels. The following patents are also concerned with methods for accelerating the cure of phenolic resole resins: US-A-4,373,062 of 2/8/83 to Brown which uses a phenol-formaldehyde resole resin to which resorcinol is added and subsequently cured with formaldehyde; and US-A-4,977,231 of 12/11/90 to McVay which discusses shortcomings of phenolic resole resins including the use of ester functional curing agents such as propylene carbonate. McVay uses certain carbamate catalysts to solve the problem of slow cure.

[0004] Kirk-Othmer, Encyclopedia of Chemical Technology, Third Edition, Volume 13, pages 58 and 59 describes resorcinol adhesives as room temperature curing and water resistant and states that resorcinol-formaldehyde and resorcinol modified phenol-formaldehyde resins are used to laminate wood. Also, Knop and Pilato, Phenolic Resins, 1985, page 13, states that resorcinol or resorcinol-formaldehyde prepolymers can be used as accelerating compounds for curing phenolic resins and that the addition of 3% to 10% of such compounds permits a shorter cure cycle in the manufacture of particle board.

[0005] Resorcinol is very expensive in relation to phenol and mixtures of resorcinol resin in monohydroxylic phenolic resole resins are not efficient from the standpoint of the increase in performance in relation to the amount of resorcinol resin needed. Additionally, for curing of such resins prepared from both resorcinol and phenol, the prior art added formaldehyde or para-formaldehyde to the mixture.

[0006] Resorcinolic resins will not cure without the addition of an alkylene donor such as a methylene donor, e.g., formaldehyde or hexamethylenetetramine (hexamine). However, with such a methylene donor, resorcinolic resins have the ability to cure at room temperature and at elevated moisture contents. Resorcinolic resins are made with a deficiency of formaldehyde so as to be stable until the time of use, at which time sufficient formaldehyde or other methylene donor is used to cure the resin. A two part adhesive containing a resorcinolic resin is described in Patent Abstracts of Japan, vol 15, no. 154 of JP-A-3031384 which discloses a two pack resorcinol-based resin adhesive which comprises, in one pack, an acid catalysed resorcinol formaldehyde condensate and, in the other pack, a hardener component containing liquid phenolic resin preferably containing free formaldehyde. By mixing the contents of the two packs together the adhesive composition is produced.

[0007] Another source of methylene donors for resorcinolic resins is a class of chemicals called oxazolidines. These can be reaction products of formaldehyde and certain amino alcohols derived from nitroparaffins. The oxazolidines react with resorcinolic resin solutions which lack formaldehyde, in the manner of formaldehyde, without actually releasing formaldehyde to the solution or to the atmosphere. The use of oxazolidine to catalyze resorcinolic resins, including phenol-resorcinol resins is shown in the following US patents: US-A-3,256,137 of 6/14/66 to Danielson; US-A-3,281,310 of 10/25/66 to Danielson; US-A-3,698,983 of 10/17/72 to Bryant; US-A-3,705,832 of 12/12/72 to Stephan; and US-A-3,517,082 of 6/23/70 to Cockerham. Technical Review, TR No. 4 of the Angus Chemical company also

describes oxazolidines as useful curing additives of phenol-formaldehyde and one stage phenolic resins.

[0008] In this invention, Part One, of the two-part adhesive of this invention comprising the methylene donor and the alkaline monohydroxylic phenolic resole resin are stable. Part Two which comprises the resorcinolic resin and optionally the catalyst for the resole resin of Part One is also stable. On mixing of the two parts the methylene donor of Part One catalyzes the resorcinolic resin of Part two and when Part Two also contains a catalyst for the resole resin such catalyst catalyzes the resole resin of Part One. The mixture of the Part One and Part Two components, i.e. the adhesive, is applied to lignocellulosic material in the manufacture of composition board which is eventually pressed and heated to cure the adhesive.

SUMMARY OF THE INVENTION

[0009] The problem solved by applicants involves methods and compositions for efficiently, conveniently and economically accelerating the cure of monohydroxylic phenolic resole resins without release of formaldehyde while improving properties of lignocellulosic panels prepared with the adhesive. Such properties are better than those when the resin is used alone and more efficient and convenient than the prior art mixture of resins or copolymers containing resorcinol. This invention allows lower resin usage levels than with a conventional monohydroxylic phenolic resole resin or a resorcinolic resin. There is a synergy in the approach of this invention which yields unexpectedly high adhesive properties at moderate expense.

[0010] This invention provides cure times when manufacturing lignocellulosic panels which are much faster than conventional phenolic resole resins when the Part One component contains a methylene donor irrespective of whether the Part 2 component contains a catalyst for the resole resin. When the Part Two component contains a catalyst for the resole resin of Part One, the cure times are essentially equivalent to that of polymeric isocyanate. The adhesive compositions of this invention are also capable of curing under high moisture and low temperature conditions.

[0011] In one aspect of this invention there is provided an adhesive prepared from two parts wherein one part, referred to as Part One, comprises a stable mixture of a monohydroxylic phenolic resole resin with a methylene donor. The methylene donor in Part One does not emit formaldehyde fumes from the resole resin. The other part, referred to as Part Two, comprises a stable mixture of a resorcinolic resin with a catalyst for the resin of Part One. When the two parts are mixed together, the catalyst of each part polymerizes the resin of the other part.

[0012] In still a further aspect, the invention comprises lignocellulosic panels prepared by mixing the above mentioned adhesive parts and applying the mixture to lignocellulosic components which are subsequently subjected to heat and pressure to cure the resins and form the bond for the panels.

[0013] Additional aspects include methods for the preparation and use of the above mentioned compositions and articles.

[0014] The methods and compositions of this invention provide additional advantageous properties such as: good lignocellulosic board properties; high curing speed with relatively small quantities of resorcinol; moisture tolerance; use of small quantities of total resin; good handling properties of the resin; greater binder efficiency in that lower quantities of the mixed adhesive can be used as compared to a resole resin.

[0015] Resorcinolic resins need a cross-linker such as formaldehyde to cure but adding formaldehyde to a resorcinolic resin causes fuming and other problems. Use of the methylene donors of this invention which are stable in the resole resin, overcome such problems.

DETAILED DESCRIPTION OF THE INVENTION

The Alkaline Monohydroxylic Phenolic Resole Resin

[0016] The monohydroxylic phenolic resole resin, also referred to herein simply as resole resin, can be any conventional aqueous alkaline resole resin solution made with a monohydroxylic phenol suitable for use as an adhesive in the manufacture of oriented strandboard or the like composite boards. By the term monohydroxylic is meant that there is only one hydroxyl group attached to an aromatic carbon ring. This is in contrast to dihydroxylic which has two hydroxyl groups attached to the aromatic carbon ring, e.g., such as with resorcinol. Such monohydroxylic resole resins can be high or low condensed resins. Typical resins include saturating resins, hardboard resins, particleboard resin, plywood resin, fiberboard resins, strandboard resins, glass binder, or other industrial monohydroxylic resole resins.

[0017] The resole resins may be obtained by the reaction of phenol, cresols, 3,5-xyleneol, bisphenol-A or other monohydroxylic substituted phenols or mixtures thereof with aldehydes such as formaldehyde, acetaldehyde or furfuraldehyde. These resins are referred to as aqueous since the solids are dissolved in water or water together with minor amounts, e.g., less than about 5% or 10% by weight of a non-reactive solvent such as alkanols of 1 to 4 carbon atoms or glycols of about 2 to 4 carbon atoms.

[0018] The reaction in the manufacture of the monohydroxylic phenolic or such phenolic derivative with aldehyde for

production of the resole resin used in this invention takes place in the presence of alkaline materials such as sodium hydroxide, potassium hydroxide or ammonia. The preferred resole resin is the condensation product of phenol and formaldehyde or wherein only a portion such as less than half of the phenol or formaldehyde is substituted with another monohydroxylic phenolic derivative or other aldehyde.

[0019] Typically, the molar ratio of formaldehyde or other aldehyde to phenol or other monohydroxylic phenolic derivative in the resole resin is about 1:1 to 3:1 and preferably from about 1.8 to 2.5 moles of the aldehyde for each mole of the phenol or monohydroxy phenolic derivative. The resole resin has an alkalinity content, i.e., contains a base, in the range of 0.5% to about 15%, and preferably 1% to 12%, based on the weight of the resin solution, when the base is sodium hydroxide. Thus, the term "alkalinity content" or simply "alkalinity" is based on sodium hydroxide solids. When a different base is used, the alkalinity content is proportionally equivalent on a molar weight basis. For example, to attain a 4% sodium hydroxide equivalent weight alkalinity content, it requires 4 grams of sodium hydroxide in 100 grams of resin solution, but 5.61 grams of potassium hydroxide in 100 grams of the resin are required to attain the same alkalinity content. Additional base can be added to a resole resin after manufacture in order to bring it to the desired alkalinity content. The pH of the resole resin will be at above 8, preferably above 9, and particularly above 10.

[0020] The resole resin used in this invention will have a resin pan solids content of about 20% to 75% by weight and preferably about 45% to 60%. Generally, the viscosity should be such as to permit the solution to be sprayed on the cellulosic components such as flakes or strands or to otherwise be applied to the components such as veneer. Thus, the viscosity of the resole resin component will generally vary from about 50 to about 1,000 centipoise (0.05 to 1 Pas) at 25°C as determined by a Brookfield RVF viscosimeter with a number 2 spindle at 20 revolutions per minute at 25°C and preferably from about 100 to 300 cP (0.1 to 0.3 Pas) at 25°C when used with particulate components such as strands.

[0021] The free formaldehyde in the resole resin used in this invention will typically be less than about 0.3% and preferably less than about 0.1% by weight of the resin.

[0022] A typical resole resin which can be used in this invention can be prepared as follows: To a clean reactor, charge 26 parts of phenol, 36.5 parts 50% formaldehyde in water, 17.5 parts water, and 6 parts 50% sodium hydroxide in water, all by weight. Heat the mixture to 90°C and react to 500 cP (0.5 Pas) Brookfield viscosity, when measured at 25°C. Cool to 75°C and charge 6 parts of 50% sodium hydroxide. React to 600 cP (0.6 Pas) at 25°C Brookfield. Cool to room temperature. Charge 8 parts urea, and mix until dissolved. Finished specifications would be: 50% resin solids; 6% alkalinity; viscosity of 100-200 cP (0.1 to 0.2 Pas) at 25°C; and a molar ratio of 2.2 moles of formaldehyde for each mole of phenol.

The Resorcinol Resin

[0023] The resorcinolic resins used in this invention are made with an aldehyde to resorcinol molar ratio of 0.2 to 1.0 and preferably about 0.5 to 0.8 moles of aldehyde per mole of resorcinol. Illustrative of aldehydes which can be used there can be mentioned formaldehyde and acetaldehyde. Sodium hydroxide or other alkaline catalysts as well as modifiers such as those listed with the monohydroxylic phenolic resole resins are generally used in the manufacture of the resorcinolic resins. In addition to the resorcinol and aldehyde, the resorcinolic resins can also contain monomers copolymerizable therewith such as phenol. The quantity of phenol copolymerized in the resorcinolic resin can vary over a broad range. Thus, as much as 60 parts by weight of phenol based on 50 parts of resorcinol can be copolymerized in the resorcinolic resin. When phenol is copolymerized with the resorcinol, the quantity of aldehyde used for reacting with the phenol is about the same as that set forth above for the resorcinol. Generally, the quantity of phenol is the resorcinolic resin will be no more than equal to that of the resorcinol. Preferably the quantity of phenol is less than 25 and particularly less than 10 parts of phenol for each 50 parts of resorcinol.

[0024] The resorcinolic resins are described as precondensates or partially reacted since they need additional formaldehyde or methylene groups to cure. The pH of the resorcinolic resin will vary from 6 to 9 and preferably from about 6.5 to 8.5.

[0025] The viscosity of the resorcinolic resin can vary over a wide range such as that of from about 40 to 1000 cP (0.04 to 1 Pas) at 25°C. For use with particulate components such as strands, the viscosity will generally vary from about 50 to about 300 cP (0.05 to 0.3 Pas) at 25°C. For use with veneers, the viscosity will generally be higher up to about 1,000 cP (1 Pas) at 25°C. Since the resorcinolic resin is made with a deficiency of aldehyde, such resin gains viscosity to a certain point and then stops. The point at which viscosity increase ceases is generally determined by the aldehyde to resorcinol molar ratio.

[0026] The resorcinolic resins used in this invention can be those which are used for laminating wood and in the manufacture of structural wood products. Such resins are preferably made with formaldehyde but other aldehydes such as acetaldehyde or furfuraldehyde can be used.

[0027] A resorcinolic resin useable in this invention to which a catalyst for the resole resin is added can be prepared as follows: To a clean reactor, charge 21 parts of water, 33 parts of resorcinol and about 0.75 parts of a 50% aqueous

sodium hydroxide solution and heat the mixture to about 55°C. Ten and one-half parts of an aqueous solution containing 50% of a formaldehyde is added slowly at about 55°C to 60°C. Additional solution of sodium hydroxide (50% in water), 2.3 parts, and 14 parts of water are added and the mixture is heated to 80°C to 85°C until the viscosity stabilizes. The solution is then cooled and 17 parts of triacetin and one part of propylene glycol are added. All parts and percentages are by weight. This resorcinolic resin will have: a molar ratio of about 0.71 moles of formaldehyde per mole of resorcinol; a pH of about 7.2 to 7.8; a Brookfield viscosity of about 70 to 100 cP (0.07 to 0.1 Pas) at 25°C; and about 50% solids.

[0028] When catalyst is in the composition of the Part Two resorcinolic resin, the resulting mixture is stable in that the catalyst will not promote cross-linking of the resorcinolic resin. Also, the catalyst itself is relatively stable in the resin although there is some degradation of the catalyst with time. The mixture of resorcinolic resin and catalyst of Part Two is stable over a period of weeks or more.

Methylene Donors for the Resorcinolic Resin

[0029] Illustrative of methylene donors, also referred to as formaldehyde donors or cross-linking agents, which are placed in the Part One component of the adhesive and which do not affect stability of the resole resin and do not fume in such resin, there can be mentioned materials which have a methylol group as well as materials which do not have a methylol group.

[0030] Illustrative of such methylene donors which do not have a methylol group there can be mentioned: trioxane; hexamine; ethylene diamine/formaldehyde product such as 1,4,6,9-tetrazatricyclo-(4.4.1.1)-dodecane; cyclic triformals such as ethyleneamine triformal, and triformaldehyde glycerine ester; as well as certain oxazolidines.

[0031] Illustrative of such methylene donors which have a methylol group there can be mentioned: methylolated mono- and dialkylamines such as methylol methylamine (methylaminomethanol), or dimethylaminomethanol; methylolated amides such as mono- and dimethylol formamide, methylol acetamide, or N-methylolacrylamide; methylolated imides such as N-methylol succinimide or N-methylol phthalimide; methylolated polyamides such as N-methylol polyhexamethylene adipamide; methylolated urethane; methylolated protein; urea-formaldehyde complexes such as methylolated ureas, e.g., monomethylolurea and dimethylolurea, methylolated condensed urea such as methylolated methylene diurea and methylolated substituted ureas such as methylol dimethyl urea; methylolated phenol; methylolated melamine, or melamine precursors such as dicyandiamide; methylolated thiourea, and condensed thiourea such as methylol methylenethiourea; methylolated nitromethane; dimethylol glycine anhydride; and methylol hydantoin; as well as certain oxazolidines. The term urea-formaldehyde complexes as used herein refers to low molecular weight combinations of urea and formaldehyde in contrast to resinous urea-formaldehyde

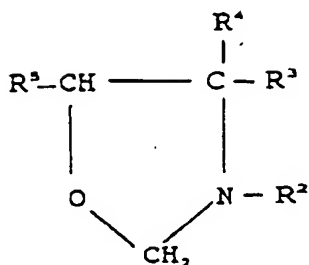
[0032] In preparing the Part One component there is added to the resole resin an amount of methylene donor necessary to crosslink the resorcinolic resin. This amount can vary from 0.3% to 15% by weight of the liquid resole resin, preferably in the range of 0.8% to 10% and particularly about 1% to 5%. The methylene donor will not catalyze the resole resin and the mixture exhibits viscosity stability typical of an unmodified monohydroxylic resole resin. The methylene donor itself is stable in the Part One resin. This is in contrast to methylene donors such as formaldehyde and paraformaldehyde which fume and release formaldehyde to the environment when placed in the resole resins used in this invention. A preferred way for preparing Part One component is to prepare the methylene donor in situ as part of the manufacture of the resole resin. This is easily accomplished by adding excess formaldehyde during the manufacture or at the end of the manufacture of the resole resin and further adding urea to the resole resin so as to react with the excess formaldehyde.

The Oxazolidine Methylene Donor

[0033] Preferred classes of methylene donors are the oxazolidines and urea-formaldehyde complexes. Any oxazolidine can be used in this invention as long as it has minimal or no effect on the stability of the aqueous monohydroxylic phenolic resole resin of Part One and reacts with the resorcinolic resin on mixing of the Part One and Part Two components of the adhesive.

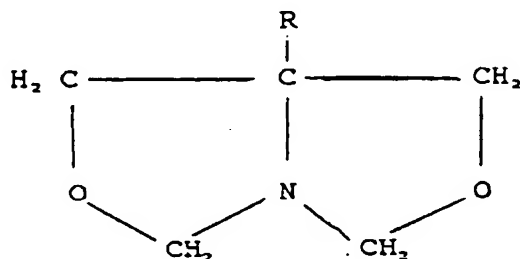
[0034] A review of oxazolidine chemistry appears in Chemical Reviews 53, 309-352 (1953). Illustrative of suitable oxazolidines there can be mentioned the various 1,3-oxazolidines shown in U.S. Patent 3,281,310 of Oct. 25, 1966 to Danielson; and those of U.S. Patent 3,256,137 of June 14, 1966 to Danielson.

[0035] The compounds of the 3,281,310 patent wherein the nitrogen is part of only one ring can be represented the formula:



wherein R^2 is hydrogen, alkyl of 1 to 8 carbon atoms, hydroxyalkyl of 1 to 8 carbon atoms, benzyl, or phenylcarbamyl, and each of R^3 , R^4 , and R^5 is hydrogen or an alkyl of 1 to 8 carbon atoms. Illustrative of such oxazolidines there can be mentioned: 4,4-dimethyl-1,3-oxazolidine; 3-(2-hydroxyethyl)-1,3-oxazolidine; 3-(2-hydroxypropyl)-5-methyl-1,3-oxazolidine; 5-methyl-1,3-oxazolidine; 3-ethyl-1,3-oxazolidine; 3-benzyl-1,3-cyclohexyl-5-methyl-1,3-oxazolidine; 3-phenylcarbamyl-4,4-dimethyl-1,3-oxazolidine; as well as the corresponding bis(1,3-oxazolidino)methanes such as bis(4,4-dimethyl-1,3-oxazolino)methane.

[0036] The oxazolidine compounds of the 3,256,137 patent wherein the nitrogen is directly attached to a first and a second ring of a bicyclic heterocycle can be represented by the formula:



wherein R is hydrogen, methyl, ethyl, n-propyl, isopropyl, methylol, beta-hydroxyethyl, acetoxymethyl or methoxymethyl. Illustrative of such oxazolidines there can be mentioned: 1-aza-3,7-dioxabicyclo[3.3.0]octane; 1-aza-5-methyl-3,7-dioxabicyclo[3.3.0]octane; 1-aza-5-ethyl-3,7-dioxabicyclo[3.3.0]octane; 1-aza-5-n-propyl-3,7-dioxabicyclo[3.3.0]octane; 1-aza-5-isopropyl-3,7-dioxabicyclo[3.3.0]octane; 1-aza-5-methylol-3,7-dioxabicyclo[3.3.0]octane; 1-aza-5-acetoxymethyl-3,7-dioxabicyclo[3.3.0]octane; and 1-aza-5-methoxymethyl-3,7-dioxabicyclo[3.3.0]octane.

[0037] The preferred oxazolidines are: 1-aza-5-ethyl-3,7-dioxabicyclo[3.3.0]octane such as that under the trademark AMINE CS-1246; 1-aza-5-methylol-3,7-dioxabicyclo[3.3.0]octane such as that under the trademark ZOLDINE ZT-55; and 4,4-dimethyl-1,3-oxazolidine such as that under the trademark AMINE CS-1135, all of which are supplied by Angus Chemical Company. The oxazolidines can be with or without a methylol group attached thereto.

Catalysts for the Alkaline Phenolic Resole Resin

[0038] Illustrative of materials which will catalyze the aqueous alkaline phenolic resole resin solution of Part One, there can be mentioned organic ester functional catalysts as well as carbamates. Thus, to the resorcinolic resin of the Part Two component is added a catalyst for the resole resin which takes effect on mixing of the two parts of the adhesive. The amount of catalyst can vary from 1% to 30% by weight of the resorcinolic resin but preferably in the range of 5% to 25% and particularly from about 10% to 20%. The catalyst will not catalyze the viscosity increase of the resorcinolic resin and the mixture exhibits stability typical of an unmodified resorcinolic resin.

Ester Functional Catalysts

[0039] Catalysts for the resole resin, which can be included in the Part Two component containing the resorcinolic resin, can be ester functional catalysts such as cyclic organic carbonates, lactones or carboxylic acid esters and mixtures thereof.

[0040] Examples of suitable lactones include, but are not limited to: gamma-butyrolactone; gamma-valerolactone;

beta-propiolactone; beta-butyrolactone; beta-isobutyrolactone, beta-isopentyl lactone; gamma isopentyl lactone, delta-pentyl lactone, and mixtures thereof. It is preferred to use gamma-butyrolactone.

[0041] Examples of suitable cyclic organic carbonates include: propylene carbonate; ethylene carbonate; ethylene glycol carbonate; glycerol carbonate; 1,2-butanediol carbonate, 1,3-butanediol carbonate; 1,2-pentanediol carbonate; 1,3-pentanediol carbonate; and mixtures thereof. If a cyclic organic carbonate is utilized, it is preferred to use propylene carbonate.

[0042] The carboxylic acid ester catalysts are preferably those of aliphatic esters of alcohols having about 1 to 4 carbon atoms. The alcohols can be mono-, di-, or trihydric alcohols, saturated or unsaturated and which are esterified with aliphatic acids of 1 to 4 carbon atoms which can be saturated or unsaturated, mono- or dicarboxylic. In preparing the carboxylic acid ester, the reactants should be chosen so that a long chain polyester is not formed. Aliphatic monoesters which can be used include: C₁ to C₄ alkyl propionates; C₁ to C₄ alkyl formates; C₁ to C₄ alkyl acetates; C₁ to C₄ alkyl butyrates; C₁ to C₄ alkyl pentanates. Examples of suitable carboxylic acid esters include: methyl formate; methyl acetate; ethyl acetate; methyl lactate; ethyl lactate; n-butyl acetate; butylene glycol diacetate; ethylene glycol diacetate; and triacetin (glycerol triacetate); dimethyl adipate; dimethyl glutarate; dimethyl succinate and mixtures thereof.

[0043] Generally, it is preferred to use an ester functional catalyst which contains a total of 3 to 9 carbon atoms. However, the only requirement of the ester functional curing agent is that it be dispersible in the resole resin and capable of remaining in suspension long enough to effect curing.

The Carbamate Catalysts

[0044] The carbamate catalysts for the resole resin can be a carbamate which is disclosed in US-A-4,977,231 of T. McVay et al which issued on Dec. 11, 1990. Thus, the carbamate can be a reaction product of (a) a carbonate selected from the group consisting of alkylene, glycidol, and epoxy resin carbonate and (b) ammonia. Of particular interest are the carbamates having 2 to 6 carbon atoms. e.g., hydroxyethyl carbamate or hydroxypropyl carbamate.

Resin Mixtures

[0045] The mixture of the two-part adhesive with each other can contain 1% to 30% by weight of the resorcinolic resin part (Part Two) mixed with 99% to 70% by weight of the resole resin part (Part One). Preferably, Part One will be from about 95% to about 80% of the adhesive mixture with Part Two being from about 5% to 20%. The ratio of 18% of the resorcinolic resin part, Part Two, and 82% of the resole resin part, Part One, appears to be the upper limit of economic performance under conventional hot pressing conditions. At a ratio of 15% resorcinolic resin and 85% resole resin the cure speed performance is equivalent to PMDI. At ratios lower than 15:85, performance is gradually decreased to that of a conventional resole resin at 0:100. This gives the user the ability to adjust the ratio to the cure speed performance needed. The more expensive higher mix ratio of resorcinolic resin to resole resin could be used on thick panel constructions, or with wetter wood when maximum cure speed performance is needed. The more economical lower mix ratio could be used on the inner construction when maximum cure speed is not needed.

[0046] The mixture of the two-part adhesive will have a pH of at least 8 and preferably at least 9 or 10.

Additives

[0047] Suitable additives can be used in coating the raw lignocellulosic material. Thus, from 0.25 to 3% by weight, based on the weight of the oven dry wood on the board product, of molten slack wax as well as emulsified wax can be used. Still further, from 5% to 20% by weight, based on the weight of the oven dry wood in the board product, of a suitable plasticizer may be included. Suitable plasticizers include glycol esters, glycerine esters, or phosphate esters.

[0048] Thickeners such as the various gums, starches, protein materials and clays may be used together with the resins. The resins can have additives dissolved therein. Illustratively urea is often dissolved in the resole resin in order to decrease the resin viscosity. The quantity of urea can vary over a broad range such as from about 5% to 15% based on the weight of the resole resin solution containing the urea and preferably from about 8% to 12% thereof. In addition to reducing viscosity, the urea also acts as a formaldehyde scavenger for the resole resin. In the case of phenol-formaldehyde resole resins the resin will also generally contain a small quantity of methanol, typically less than about 1% such as about 0.5% or less.

Application of the Adhesive

[0049] As is conventional in the art, the resin is applied to fibers, flakes, chips, strands and the like by various spraying techniques whereas it is generally applied to veneers by coaters. Resin applied to the lignocellulosic components is

referred to herein as a coating even though it may be in the form of small resin particles such as atomized particles which do not form a continuous coating.

[0050] The mix ratios listed above in the Resin Mixtures section allows easy handling in an in-line meter mix system as outlined in US-A-4,961,795 to Detlefsen and Phillips of Oct. 9, 1990. When used with an in-line mixer, as described in the above 795 patent, the adhesive part containing the mixture of resorcinolic resin and catalyst for the Part One component is mixed with the Part Two component containing the resole resin and cross-linking agent for the resorcinolic resin and the mixture of the two parts applied to wood strands, veneer or wood particles for the manufacture of composite board such as oriented strandboard, particleboard, fiberboard, or used for plywood construction. In some operations, however, batch mixing of the two resin components and use of the resulting mixture before the viscosity becomes excessive is possible. This can be the case in a plywood operation where fairly viscous glue mixes are used.

[0051] The resulting mixed adhesive has a very short boiling water gel time when compared to a conventional resole resin. The ratio of the two resins in the adhesive mixture can be varied to obtain the level of catalysis required. At a blend ratio of 85 parts of the Part One component and 15 parts by weight of the Part Two component the resulting adhesive has hot press cure times equivalent to PMDI.

[0052] The mixture of Part One and Part Two adhesive can be applied to the wood with any form of conventional equipment currently in use. Such equipment includes spray nozzles, atomizing wheels, roll coaters, curtain coaters and foam applicators. It is important for successful use, however, in obtaining a relatively short time interval between mixing of the two parts of the adhesive and application of the mixture to the wood. This is because the viscosity of the mixture begins to rapidly increase and may result in loss of solubility in water and base shortly after mixing. For these reasons, in-line mixing of the first and second parts of the adhesive just prior to application to the wood is preferred.

[0053] The range of resin solids for the total of resorcinolic resin and the resole resin from the two components before curing which are applied to the lignocellulosic components can vary from about 1% to 15% by weight of the lignocellulose depending on the quality of the panel product desired. Preferably, the amount of binder can vary from about 2% to about 8% of resin solids in each of the components based on the weight of the lignocellulose being bound. The resin solids includes the catalysts.

[0054] Hot pressing conditions for the panels utilizing the two-part adhesive of this invention will depend on the thickness of the board, the type of board, as well as on the resin characteristics. Generally, the platen temperatures can vary from about 240°F to 420°F (115° to 216°C) at pressures of about 75 to 250 psi (517 to 1724 kPa) for about 2 to 10 minutes.

The Lignocellulosic Materials

[0055] The lignocellulosic materials which are the basic raw materials for panels which can be made from the adhesive of this invention may be derived from a large number of natural sources. They may be derived, for example, from sugar cane bagasse, straw, cornstalks, and other waste vegetable matter. In particular however, they are derived from various species of wood in the form of wood fibers, chips, shavings, flakes, particles and veneers. These materials which are used to prepare the panels are referred to generally herein as lignocellulosic components. The manufactured products including hardboard, particleboard, fiberboard, waferboard, strandboard and the like as well as plywood, laminated veneer lumber or laminated wood particles. The internal bond strength of these products will be at least about 30 psi (207 kPa).

[0056] The invention will be demonstrated by the following examples. In these examples and elsewhere through the specification, parts and percentages are by weight unless expressly indicated otherwise. Also, the term "resin solids" refers to pan solids according to an industry accepted test where one gram of resin is placed in an aluminium pan and heated in a forced air oven at 125°C for one hour and 45 minutes. Such solids include catalysts, e.g., esters and carbamates as well as methylene donors such as oxazolidine and urea-formaldehyde complexes.

Procedures and Examples.

[0057] Boiling Water Gel Tests. The boiling water gel tests to determine gel time were conducted with a Gel Time Meter, Catalog No. 22 of Sunshine Scientific Instrument of 1810 Grant Avenue, Philadelphia, Pa. The gel-time meter essentially consists of a motor-driven, rotating spindle suspended in the test sample. The sample is maintained at constant temperature by a boiling bath surrounding the sample cell. In this case, the boiling bath was that of water so that the temperature was 100°C. At the gel point, the very pronounced increase in viscosity of the sample stops the rotating spindle, closing an electrical switch which actuates the timing and alarm circuits. In operation, the sample tube containing a 10 gram sample, unless otherwise indicated, and the spindle are placed in the briskly boiling water bath. At the same time, the power switch is turned on, starting the counter and the slowly rotating spindle device. The spindle is locked into the spindle drive by magnetic coupling. The test switch is turned on, setting up the automatic counter stop and alarm circuits. The instrument needs no further attention for the duration of the test. When the gel point is

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reached, the increased viscosity of the test sample stops the rotating spindle and the actuating switch is closed. This switch shuts off the spindle motor and the counter, and actuates the visible and audible signal. The gel time and the bath temperature are then recorded by the operator, and the test is complete.

EXAMPLE 1

[0058] This example illustrates preparation of the two-part adhesive wherein the first part is that of a mixture of an aqueous alkaline monohydroxylic phenolic resole resin solution (PF) and an oxazolidine and the second part is phenol-resorcinol-formaldehyde co-condensed aqueous resin solution (PRF) without ester catalyst for the resole resin. The resole resin is referred to as WS474-101 and is made with phenol, formaldehyde, water, and sodium hydroxide, with 7.2% urea added in the finished polymer. The pH of this resole resin was 11.95. AMINE CS 1246, namely, 1-aza-5-ethyl-3,7-dioxabicyclo(3.3.0)octane, an oxazolidine supplied by Angus Chemical Company, is added to attain a 10% by weight concentration in the resin. The final resin has a pan solids of 51%, an alkalinity of 7% NaOH, molar ratio of 2.25:1 of formaldehyde to phenol, and 150 cP (0.15 Pas) Brookfield viscosity. The phenol-resorcinol resin, referred to as WS453-88, is made with phenol, resorcinol, formaldehyde, water and sodium hydroxide. The resulting resorcinolic resin has pan solids of 50%, alkalinity of 3.5% NaOH, a molar ratio of 0.95:1 of formaldehyde to phenol-resorcinol, and 200 cP (0.2 Pas) Brookfield viscosity.

EXAMPLE 2

[0059] This example shows a two-part adhesive wherein the first part is that of an aqueous alkaline monohydroxylic phenolic resole resin solution and the second part is an aqueous polymerizable resorcinolic resin (RF) wherein each part carries a catalyst for the other part. The resole resin (PF), referred to as WS421-110, is made with phenol, formaldehyde, water, and sodium hydroxide, with urea added to the finished polymer to provide a resin having 10.8% urea and a pH of 12. ZOLDINE ZT55, namely, 1-aza-5-methylol-3,7-dioxabicyclo(3.3.0)octane, an oxazolidine supplied by the Angus Chemical Company, is added within the preferred range. The final resin, including the oxazolidine and urea has pan solids of 50%, alkalinity of 7% NaOH, molar ratio of 2.3:1 of formaldehyde to phenol, and a viscosity of 110 cP (0.11 Pas) at 25°C Brookfield viscosity. Part two is a resorcinolic resin, referred to as WS421-109, which is made with resorcinol, formaldehyde, water, and sodium hydroxide. Triacetin, an ester, is added to the resorcinolic resin to provide a resin having 17% of triacetin. The resorcinolic resin had pan solids of 51%, alkalinity of 1.5% NaOH, a molar ratio of 0.58:1, formaldehyde to resorcinol, a pH of 7.6, and a viscosity of 80 cP (0.08 Pas) at 25°C Brookfield viscosity.

EXAMPLE 3

[0060] Different ratios of the two stable resin-catalyst mixtures from Example 2 were tested to determine boiling water gel time. The samples were hand mixed immediately before testing. The tests were run on 5 gram samples of the resin catalyst mixtures using a Sunshine Gel Meter with boiling water as the heating medium. The results of this example are shown in Table 3 wherein the column on the left shows the resorcinol-formaldehyde part to phenol-formaldehyde resole part proportions in parts by weight and the right hand column shows the gel time in minutes (min).

Table 3

RF : PF	Boiling Water Gel Test
0 : 100	28 min.
5 : 95	13.1 min.
10 : 90	4.8 min.
15 : 85	1.7 min.
20 : 80	1.5 min.

[0061] It can be seen from Table 3 that the mixture of resorcinol-formaldehyde resin and ester catalyst is very effective in reducing the gel time of the system to the point where factors other than the catalytic effect such as heat transfer into the sample, become controlling.

Example 4

[0062] Laboratory strandboards were made with the phenolic resole resin mixture of Example 1, also referred to as PF in Table 4, with the resorcinolic resin of Example 1, also referred to as PRF in Table 4. These were mixed in the

ratio of 50:50 by weight. The pH of the mixed resins was at least about 10. Resole Resin A was also tested for comparison purposes and as a control. Resin A is an aqueous solution of phenol-formaldehyde resole resin having: a molar ratio of about 2.2 moles of formaldehyde per mole of phenol; 47% solids; Brookfield viscosity of about 200 cP (0.2 Pas) at 25°C; a pH of about 12.5; less than 0.5% of free phenol; less than 0.2% of free formaldehyde; which was made with sodium hydroxide as the base and which contains 8% of urea which was added after the resin cooled. The dimensions of the boards were 14 × 14 × 0.75 inches (36.5 × 36.5 × 1.9 cm). They were pressed in an oil-heated laboratory hot press set at 390°F. (199°C). Target board density was 40 pcf, and the wood was southern pine strands with minor amounts of mixed southern hardwoods. The wood moisture before resin application was 9% and 14% after resin application. The boards had random strand orientation, and were homogeneous in construction. The resins were mixed by hand just prior to use and applied to the strands in a laboratory rotating blender using air atomization. The resins were applied at the rate of 5% resin solids to dry wood weight. Press cycle times, including press closing and board degas, were adjusted to determine cure speed of the resins. This was done by examining board edges and corners for weakness immediately out of the press. The results of this example are shown in Table 4 wherein the first three series of results are for the Resin A and the second three series are for the mixture of the two-part adhesive of Example 1.

Table 4

Resin	Cycle	IB		MOR		6-Cycle MOR		TS
	(min)	(psi)	(kPa)	(psi)	(kPa × 10 ²)	(psi)	(kPa × 10 ²)	
Resin A	7.5	39	(269)	2971	(205)	1296	(89)	12.7
	7.0	46	(317)	2033	(140)	1711	(118)	11.4
	6.5	26	(179)	1780	(123)	1389	(96)	13.2
PRF : PF 50 : 50	5.0	39	(269)	2852	(197)	1452	(100)	10.5
	4.5	40	(276)	2648	(183)	1793	(124)	11.0
	4.0	26	(179)	2049	(141)	1527	(105)	12.6

[0063] The data of the above Table 4 show that the inventive mixture of this invention is much faster curing than the control commercial resin, which is the fastest curing conventional monohydroxylic phenolic resole resin that the supplier of that resin markets. In the above Table 4, IB refers to internal bond, MOR refers to modulus of rupture, 6-cycle MOR refers to modulus of rupture after six cycles of soaking and drying (durability), and TS refers to thickness swell after 24 hours cold soak in water.

EXAMPLE 5

[0064] Laboratory strandboards were made with the resins from Example 2 mixed in various ratios by weight, using a monohydroxylic phenolic resole resin solution designated as Resin B as a control resin. The pH of the mixture of resins was about 10 to 11. Resin B has a molar ratio of about 2.2 moles of formaldehyde per mole of phenol; 47% solids; Brookfield viscosity of about 100 cP (0.1 Pas) at 25°C; a pH of about 13; less than 0.5% free phenol; less than 0.1% of free formaldehyde; and which was made with sodium hydroxide as the base. Resin B contains 9.4% formaldehyde which was added after the condensation of the phenol and formaldehyde. The boards were manufactured as in Example 4, except that a press temperature of 400°F (204°C) was used, and wood moisture was lower, i.e., 3% before resin application.

Table 5

Adhesive	Cycle	IB		MOR		6-CYCLE MOR	
	(min)	(psi)	(kPa)	(psi)	(kPa × 10 ²)	(psi)	(kPa × 10 ²)
Resin B	6.0	69	(476)	3516	(242)	1358	(94)
	5.5	58	(400)	3164	(218)	1817	(125)
	5.0	45	(310)	2520	(174)	1165	(80)
	4.5	29	(200)	1659	(114)	1268	(87)
RF : PF	4.5	73	(503)	3298	(227)	1927	(133)

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Table 5 (continued)

Adhesive	Cycle	IB		MOR		6-CYCLE MOR	
	(min)	(psi)	(kPa)	(psi)	(kPa × 10 ²)	(psi)	(kPa × 10 ²)
12 : 88	4.0	73	(503)	3916	(270)	2234	(154)
	3.5	58	(400)	3157	(218)	1863	(128)
	3.0	45	(310)	2452	(169)	1640	(113)
RF : PF	4.5	77	(531)	3059	(211)	2153	(148)
15 : 85	4.0	68	(469)	3479	(240)	1971	(136)
	3.5	63	(434)	3161	(218)	1651	(114)
	3.0	46	(317)	2614	(180)	1918	(132)
RF : PF	4.5	75	(517)	3732	(257)	2174	(150)
18 : 82	4.0	79	(545)	3620	(250)	2054	(142)
	3.5	66	(455)	3497	(241)	2034	(140)
	3.0	58	(400)	3021	(208)	2026	(140)

[0065] The data of the above Table 5 show that the examined range of experimental mix ratios were all much faster curing than the control resin. They also show that higher ratios of the resorcinol component give better bonding at the shortest press cycles.

EXAMPLE 6

[0066] Laboratory boards were made as in Example 5 with the following changes: aspen strands were used with moisture content of 9-10% before resin application; press temperature was 260°F; (127°C); Resin A, which was also used in Example 4, was again used as a control. Wood moisture was 14% after resin application. The results of this example are shown in Table 6.

Table 6

Adhesive	Cycle	IB		MOR		6-CYCLE MOR	
	(min)	(psi)	(kPa)	(psi)	(kPa × 10 ²)	(psi)	(kPa × 10 ²)
Resin A	13	37	(255)	2840	(196)	802	(55)
	12	36	(255)	2459	(170)	790	(54)
	11	24	(165)	1492	(103)	575	(40)
	9	8	(55)	653	(45)	331	(23)
RF : PF	10	60	(414)	2760	(190)	2013	(139)
18 : 82	9	51	(352)	2932	(202)	2095	(144)
	8	47	(324)	2776	(191)	1864	(129)
	7	29	(200)	2178	(150)	1331	(92)

[0067] The data of the above Table 6 show that the experimental adhesive of the invention is very moisture tolerant, and will cure at low press temperature, even at short press cycles.

EXAMPLE 7

[0068] In this example, tests were made to compare oxazolidine with hexamine (hexamethylenetetramine) as formaldehyde donors. This was done by noting the time for the boiling water gel test of Sample 1 which contained 85 parts of Component A and 15 parts of Component E with Sample 2 which contained 85 parts of Component B and 15 parts of Component E. The composition of these various Components is described below. As can be seen from the first part of Table 7, there was about the same degree of catalysis when the hexamine was used on an equivalent basis

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with the ZT-55 (oxazolidine). Also, in the second part of this example, tests were made with methylolurea as the formaldehyde source. The resole resin (Component C) contained about 0.1% of free formaldehyde. It can be seen from a comparison of Sample 3 and Sample 4 in Table 7 that combining the resole resin of Component C with the resorcinolic resin of Component F gave a shorter Boiling Water Gel time. When 15 parts of resorcinolic resin, (Component F) was mixed with 85 parts of Component D which is the resole resin which included 5% of the fifty percent aqueous formaldehyde solution and 10% of urea, the boiling water gel time was down to 2.2 minutes. In Sample 6, which had a mixture of 85 parts of the resole resin containing methylolurea from the reaction of urea and formaldehyde (Component D) and 15 parts of the resorcinolic resin containing triacetin (Component E), the boiling water gel time was only one minute.

Component

[0069]

- A WS421-110 containing 2.22% of ZT-55 oxazolidine which in turn is a 43% solution of the oxazolidine in water.
- B WS421-110 containing 3.00% hexamine solution which in turn is a 43% solution of the hexamine in water.
- C This is a monohydroxylic phenolic resole resin of phenol and formaldehyde having 43% pan solids, a pH of 11.7 and a nominal viscosity of 750 cP (0.75 Pas) at 25°C.
- D This is the resin of Component C above plus 5% of 50% aqueous formaldehyde and 10% of urea.
- E WS421-109 (resorcinolic resin described in Example 2) together with 3% triacetin as catalyst for the resole resin.
- F WS421-109 without ester of Component E above.

Hexamine		
Sample	Components	Boiling Water Gel Time
1	A 85 parts E 15 parts	1.3 minutes
2	B 85 parts E 15 parts	1.2 minutes

Methylolurea		
3	C 100 parts	25 minutes
4	C 80 parts F 12.5 parts	19.9 minutes
5	D 85 parts F 12.5 parts	2.2 minutes
6	D 85 parts E 15 parts	1.0 minute

Example 8

[0070] In this example boiling water gel tests were made to show the synergism of the cross-catalysis. In this example, boiling water gel tests were made on each of the resole and resorcinolic resins alone carrying catalysts for the other part as well as combinations of such resins and catalysts. The designator PF in Table 8 is the WS421-110 base resin of Example 2 above with no methylene donor and the designator RF is the WS110-109 base resin of Example 2 above with no catalyst. The amount of each catalyst or methylene donor employed in Table 8 is the same as that in Components A and E of Example 7 above at a mix ratio of 15 parts of the resorcinolic resin and 85 parts of the resole resin.

Table 8

Sample	Boiling Water Gel Time
1 PF + oxazolidine	29.1 minutes
2 PF + triacetin	11.3 minutes
3 PF + RF + oxazolidine	3.3 minutes
4 PF+ RF +oxazolidine + triacetin	1.3 minutes

Example 9

[0071] Tests were made for boiling water gel time by adding various chemicals to resorcinolic resin WS421-126 which of itself has no boiling water gel time. The results of these tests are shown in Table 9 below.

Table 9

Additive	Percent Addition	Boiling water Gel Time
Dimethylolurea	20%	1.9 minutes
N-Methylolacrylamide	15%	11.4 minutes
Tris-hydroxy-methyl-nitromethane	20%	3 minutes.

Claims

1. A method for preparing an adhesive composition from two components which comprises forming a mixture by mixing:

A. A first component comprising a stable aqueous alkaline monohydroxylic phenolic resole resin solution containing a methylene donor selected from compounds which do not have a methylol group and compounds which have a methylol group; with
 B. a second component comprising a stable aqueous resorcinolic resin precondensate having a shortage of formaldehyde and containing a catalyst for the resole resin selected from ester functional curing catalysts and carbamate catalysts; and
 C. wherein the quantity of methylene donor is in the range of from 0.3 to 15% by weight of resole resin and the amount of the catalyst for the resole resin is from 1 to 30% by weight of the resorcinolic resin.

2. The method of claim 1 wherein:

A. the quantity of the first component is from 99 parts to 70 parts by weight;
 B. the quantity of the second component is from 1 to 30 parts by weight;
 C. the pH of the resole resin is at least 9; and
 D. the pH of the resorcinolic resin is from 6 to 9.

3. The method of claim 1 wherein the methylene donor is a member selected from the group consisting of trioxane; hexamethylenetetramine; ethylenediamine/formaldehyde adducts; cyclic triformals; oxazolidine which lacks a methylol group; and methylolated compounds which act as methylene donors to resorcinolic resin precondensates which have a shortage of formaldehyde.

4. The method of claim 2 where the methylene donor is an oxazolidine with or without a methylol group as part of the oxazolidine.

5. The method of claim 2 wherein the methylene donor is a methylolurea.

6. The method of claim 2 wherein the catalyst in the second component is a carbamate.

7. The method of claim 1, wherein:

A. the ester functional curing catalyst is a member selected from the group consisting of a cyclic organic

carbonate, a lactone and a carboxylic acid ester; and

B. the carbamate is the reaction product of ammonia with a member selected from the group consisting of an alkylene carbonate, glycidol carbonate, and epoxy resin carbonate.

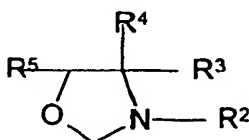
8. The method of claim 2 wherein the catalyst for the resole resin is an ester functional curing catalyst.

9. The method of claim 2 wherein the catalyst in the second component is a carbamate, said carbamate being the reaction product of ethylene carbonate or propylene carbonate with ammonia.

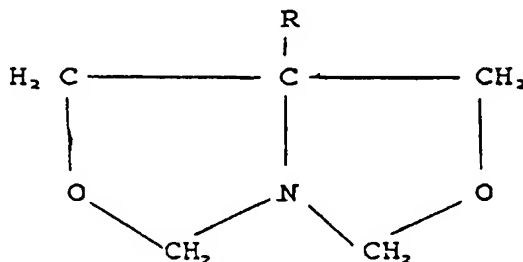
10. The method of claim 6 wherein the ester catalyst has from 3 to 9 carbon atoms.

11. The method of claim 2 wherein:

A. the methylene donor is a member selected from an oxazolidine represented by the formula



wherein R² is hydrogen, alkyl of 1 to 8 carbon atoms, hydroxyalkyl of 1 to 8 carbon atoms, benzyl, or phenyl-carbamyl, and each of R³, R⁴, and R⁵ is hydrogen or an alkyl of 1 to 8 carbon atoms; and



wherein R is hydrogen, methyl, ethyl, n-propyl, isopropyl, methylol, beta-hydroxyethyl, acetoxymethyl or methoxymethyl; and

B. the ester is a member selected from the group consisting of a lactone, a cyclic organic carbonate, a carboxylic acid ester, and mixtures thereof.

12. The method of claim 2 wherein the resole resin is the condensation product of phenol and formaldehyde.

13. The method of claim 2 wherein the resorcinolic resin is a member selected from the group consisting of: the condensation product of resorcinol and formaldehyde; and the condensation product of phenol, resorcinol and formaldehyde containing up to 55 parts by weight of phenol per 50 parts of resorcinol.

14. The method of claim 13 wherein the resorcinolic resin is the condensation product of resorcinol and formaldehyde.

15. The method of claim 13 wherein the resorcinolic resin is the condensation product of resorcinol with less than 10 parts of phenol.

16. The method of claim 11 wherein the nitrogen of the oxazolidine is part of a one ring heterocyclic.

17. The method of claim 11 wherein the nitrogen of the oxazolidine is directly attached to a first and a second ring of the oxazolidine.

18. The method of claim 17 wherein the oxazolidine is 1-aza-5-methylol-3,7-dioxabicyclo[3.3.0]octane.
19. The method of claim 17 wherein the oxazolidine is 1-aza-5-ethyl-3,7-dioxabicyclo[3.3.0]octane.
20. A method for polymerizing a monohydroxylic phenolic resole resin together with a resorcinolic resin precondensate having a shortage of formaldehyde which comprises mixing:
 - A. from 70 to 99 parts of a first component having a pH of at least 9 and comprising a stable aqueous, alkaline monohydroxylic phenolic resole resin solution containing from 0.3% to 15% based on the weight of the resole resin solution of a methylene donor selected from compounds which do not have a methylol group and compounds which have a methylol group; with
 - B. from 1 to 30 parts of a second component comprising a stable aqueous resorcinolic resin precondensate having a shortage of formaldehyde and a pH of 6 to 9 and from 1 to 30% by weight based on the weight of the resorcinolic resin of a catalyst for the resole resin selected from ester functional curing catalysts and carbamate catalysts.
21. The method of claim 20 wherein the methylene donor is an oxazolidine.
22. The method of claim 20 wherein the methylene donor is a methylolurea.
23. An alkaline adhesive composition having a pH of at least 9 and prepared by mixing:
 - A. 70 to 99 parts by weight of a first component comprising a stable aqueous alkaline monohydroxylic phenolic resole resin solution having a pH of at least 9 and containing from 0.5% to 10%, based on the weight of the solution, of a methylene donor selected from compounds which do not have a methylol group and compounds which have a methylol group; and
 - B. 1 to 30 parts by weight of a second component comprising a stable aqueous resorcinolic resin solution having a pH of from 6.5 to 8.5 and containing from 5% to 25%, based on the weight of the resin, of a catalyst for the resole resin, said catalyst selected from the group consisting of an ester functional curing catalyst and a carbamate.
24. The adhesive of claim 23 wherein the catalyst is an ester functional curing catalyst having from 3 to 9 carbon atoms selected from the group consisting of a carboxylic acid ester, a cyclic organic carbonate and a lactone.
25. The adhesive composition of claim 23 wherein the pH of the resole resin is at least 10.
26. The composition of claim 23 wherein the formaldehyde donor is methylolurea.
27. The composition of claim 23 wherein the formaldehyde donor is oxazolidine.
28. A method for the production of lignocellulosic panels by bonding lignocellulosic components under heat and pressure which comprises coating lignocellulosic components with an adhesive comprising a mixture of:
 - A. 70 to 99 parts of a first component comprising a stable aqueous, alkaline monohydroxylic phenolic resole resin solution containing from 0.3% to 15%, based on the weight of the resole resin of a methylene donor selected from compounds which do not have a methylol group and compounds which have a methylol group; and
 - B. 1 to 30 parts of a second component comprising a polymerizable resorcinolic resin containing from 1% to 30%, based on the weight of the resorcinolic resin, of a catalyst for the resole resin said catalyst selected from the group consisting of an ester functional catalyst and a carbamate which is the reaction product of a carbonate selected from the group consisting of alkylene, glycidol, and an epoxy resin carbonate with ammonia.

Patentansprüche

1. Verfahren zur Herstellung eines Klebemittels aus zwei Komponenten, umfassend das Bilden eines Gemisches durch Vermischen von

A. einer ersten Komponente, umfassend eine stabile wäßrige alkalische Lösung eines monohydroxyphenolischen Resolharzes, enthaltend einen Methylendonor, ausgewählt aus Verbindungen, die keine Methylolgruppe enthalten, und Verbindungen, die eine Methylolgruppe enthalten, mit

B. einer zweiten Komponente, umfassend ein stabiles wäßriges Resorcinharz-Prekondensat mit einem Mangel an Formaldehyd und enthaltend einen Katalysator für das Resolharz, ausgewählt aus esterfunktionellen Härtungskatalysatoren und Carbamatkatalysatoren, und

C. wobei die Menge des Methylendonors im Bereich von 0,3 bis 15 Gew.-% des Resolharzes liegt und die Menge des Katalysators für das Resolharz 1 bis 30 Gew.-% des Resorcinharzes beträgt.

2. Verfahren nach Anspruch 1, wobei

- A. die Menge der ersten Komponente 99 bis 70 Gewichtsteile beträgt,
- B. die Menge der zweiten Komponente 1 bis 30 Gewichtsteile beträgt,
- C. der pH-Wert des Resolharzes mindestens 9 ist, und
- D. der pH-Wert des Resorcinharzes 6 bis 9 ist.

3. Verfahren nach Anspruch 1, wobei der Methylendonor eine Substanz ist, ausgewählt aus der Gruppe, bestehend aus Trioxan, Hexamethylentetramin, Ethylendiamin/Formaldehyd-Addukten, cyclischen Triformalen, Oxazolidin, dem eine Methylolgruppe fehlt, und methylierten Verbindungen, die als Methylendonoren für Resorcinharz-Prekondensate dienen, die einen Mangel an Formaldehyd aufweisen.

4. Verfahren nach Anspruch 2, wobei der Methylendonor ein Oxazolidin mit oder ohne einer Methylolgruppe als Teil des Oxazolidins ist.

5. Verfahren nach Anspruch 2, wobei der Methylendonor ein Methylolharnstoff ist.

6. Verfahren nach Anspruch 2, wobei der Katalysator in der zweiten Komponente ein Carbamat ist.

7. Verfahren nach Anspruch 1, wobei

- A. der esterfunktionelle Härtungskatalysator eine Substanz ist, ausgewählt aus der Gruppe bestehend aus einem cyclischen organischen Carbonat, einem Lacton und einem Carbonsäureester, und
- B. das Carbamat das Reaktionsprodukt von Ammoniak mit einer Substanz, ausgewählt aus der Gruppe bestehend aus einem Alkylencarbonat, Glycidolcarbonat und Epoxyharzcarbonat ist.

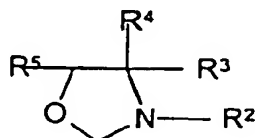
8. Verfahren nach Anspruch 2, wobei der Katalysator für das Resolharz ein esterfunktioneller Härtungskatalysator ist.

9. Verfahren nach Anspruch 2, wobei der Katalysator in der zweiten Komponente ein Carbamat ist, wobei das Carbamat ein Reaktionsprodukt von Ethylencarbonat oder Propylencarbonat mit Ammoniak ist.

10. Verfahren nach Anspruch 6, wobei der Esterkatalysator 3 bis 9 Kohlenstoffatome hat.

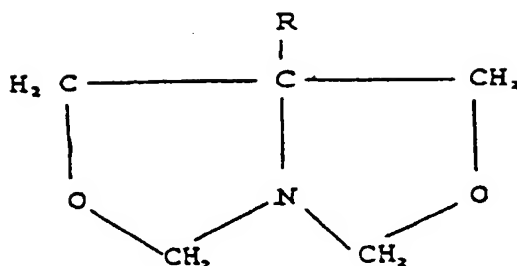
11. Verfahren nach Anspruch 2, wobei

A. der Methylendonor eine Substanz ist, ausgewählt aus einem Oxazolidin, angegeben durch die Formel



wobei R² Wasserstoff, Alkyl mit 1 bis 8 Kohlenstoffatomen, Hydroxyalkyl mit 1 bis 8 Kohlenstoffatomen, Benzyl oder Phenylcarbamy l ist und jedes von R³, R⁴ und R⁵ Wasserstoff oder ein Alkyl mit 1 bis 8 Kohlenstoffatomen

ist, und



wobei R Wasserstoff, Methyl, Ethyl, n-Propyl, Isopropyl, Methylol, β -Hydroxyethyl, Acetoxymethyl oder Methoxymethyl ist, und

B. der Ester eine Substanz ist, ausgewählt aus der Gruppe bestehend aus einem Lacton, einem cyclischen organischen Carbonat, einem Carbonsäureester und Gemischen davon.

12. Verfahren nach Anspruch 2, wobei das Resolharz das Kondensationsprodukt von Phenol und Formaldehyd ist.

13. Verfahren nach Anspruch 2, wobei das Resorcinharz eine Substanz ist, ausgewählt aus der Gruppe bestehend aus dem Kondensationsprodukt von Resorcin und Formaldehyd und dem Kondensationsprodukt von Phenol, Resorcin und Formaldehyd, enthaltend bis zu 55 Gewichtsteile Phenol pro 50 Teile Resorcin.

14. Verfahren nach Anspruch 13, wobei das Resorcinharz das Kondensationsprodukt von Resorcin und Formaldehyd ist.

15. Verfahren nach Anspruch 13, wobei das Resorcinharz das Kondensationsprodukt von Resorcin mit weniger als 10 Teilen Phenol ist.

16. Verfahren nach Anspruch 11, wobei der Stickstoff des Oxazolidins Teil eines Einring-Heterocyclus ist.

17. Verfahren nach Anspruch 11, wobei der Stickstoff des Oxazolidins direkt an einen ersten und einen zweiten Ring des Oxazolidins gebunden ist.

18. Verfahren nach Anspruch 17, wobei das Oxazolidin 1-Aza-5-methylol-3,7-dioxabicyclo[3,3,0]octan ist.

19. Verfahren nach Anspruch 17, wobei das Oxazolidin 1-Aza-5-ethyl-3,7-dioxabicyclo[3,3,0]octan ist.

20. Verfahren zum Polymerisieren eines monohydroxyphenolischen Resolharzes zusammen mit einem Resorcinharz-Prekondensat mit einem Mangel an Formaldehyd, umfassend das Vermischen von

A. 70 bis 99 Teilen einer ersten Komponente mit einem pH-Wert von mindestens 9 und umfassend eine stabile wäßrige alkalische Lösung eines monohydroxyphenolischen Resolharzes, enthaltend 0,3 bis 15 %, bezogen auf das Gewicht der Resolharzlösung, eines Methylendonors, ausgewählt aus Verbindungen, die keine Methylolgruppe enthalten, und Verbindungen, die eine Methylolgruppe enthalten, mit

B. 1 bis 30 Teilen einer zweiten Komponente, umfassend ein stabiles wäßriges Resorcinharz-Prekondensat mit einem Mangel an Formaldehyd und einem pH-Wert von 6 bis 9 und 1 bis 30 Gew.-%, bezogen auf das Gewicht des Resorcinharzes, eines Katalysators für das Resolharz, ausgewählt aus esterfunktionellen Härtungskatalysatoren und Carbamatkatalysatoren.

21. Verfahren nach Anspruch 20, wobei der Methylendonor ein Oxazolidin ist.

22. Verfahren nach Anspruch 20, wobei der Methylendonor ein Methylolharnstoff ist.

23. Alkalisches Klebemittel mit einem pH-Wert von mindestens 9 und hergestellt durch Vermischen von

A. 70 bis 99 Gewichtsteilen einer ersten Komponente, umfassend eine stabile wäßrige alkalische Lösung eines monohydroxyphenolischen Resolharzes mit einem pH-Wert von mindestens 9 und enthaltend 0,5 bis 10 %, bezogen auf das Gewicht der Lösung, eines Methylendonors, ausgewählt aus Verbindungen, die keine Methylolgruppe enthalten und Verbindungen, die eine Methylolgruppe enthalten, mit

B. 1 bis 30 Gewichtsteilen einer zweiten Komponente, umfassend eine stabile wäßrige Resorcinharzlösung mit einem pH-Wert von 6,5 bis 8,5 und enthaltend 5 bis 25 %, bezogen auf das Gewicht des Harzes, eines Katalysators für das Resolharz, wobei der Katalysator ausgewählt ist aus der Gruppe bestehend aus einem esterfunktionellen Härtungskatalysator und einem Carbamat.

24. Klebemittel nach Anspruch 23, wobei der Katalysator ein esterfunktioneller Härtungskatalysator mit 3 bis 9 Kohlenstoffatomen ist, ausgewählt aus der Gruppe bestehend aus einem Carbonsäureester, einem cyclischen organischen Carbonat und einem Lacton.

25. Klebemittel nach Anspruch 23, wobei der pH-Wert des Resolharzes mindestens 10 ist.

26. Mittel nach Anspruch 23, wobei der Formaldehyddonor Methylolharnstoff ist.

27. Mittel nach Anspruch 23, wobei der Formaldehyddonor Oxazolidin ist.

28. Verfahren zur Herstellung von Lignocellulose-Paneelen durch Binden von Lignocellulose-Komponenten unter Wärme und Druck, umfassend das Überziehen der Lignocellulose-Komponenten mit einem Klebemittel, umfassend ein Gemisch aus

A. 70 bis 99 Teilen einer ersten Komponente, umfassend eine stabile wäßrige alkalische Lösung eines monohydroxyphenolischen Resolharzes, enthaltend etwa 0,3 bis 15 %, bezogen auf das Gewicht des Resolharzes, eines Methylendonors, ausgewählt aus Verbindungen, die keine Methylolgruppe enthalten und Verbindungen, die eine Methylolgruppe enthalten, und

B. 1 bis 30 Teilen einer zweiten Komponente, umfassend ein polymerisierbares Resorcinharz, enthaltend 1 bis 30 %, bezogen auf das Gewicht des Resorcinharzes, eines Katalysators für das Resolharz, wobei der Katalysator ausgewählt ist aus der Gruppe bestehend aus einem esterfunktionellen Katalysator und einem Carbamat, das das Reaktionsprodukt eines Carbonats, ausgewählt aus der Gruppe bestehend aus Alkyl-, Glycidol- und einem Epoxyharzcarbonat, mit Ammoniak ist.

Revendications

1. Procédé pour préparer une composition adhésive à partir de deux composants, lequel procédé comprend la formation d'un mélange en mélangeant :

A. Un premier composant comprenant une solution de résine résol phénolique monohydroxylique alcaline aqueuse stable contenant un donneur de méthylène choisi parmi des composés qui n'ont pas de groupe méthylol et des composés qui ont un groupe méthylol ; avec

B. un deuxième composant comprenant un précondensat de résine résorcinolique aqueux stable ayant un déficit de formaldéhyde et contenant un catalyseur pour la résine résol choisi parmi des catalyseurs de prise à fonction ester et des catalyseurs de type carbamate ; et

C. dans lequel la quantité du donneur de méthylène est dans la fourchette de 0,3 à 15 % en poids de la résine résol et la quantité du catalyseur pour la résine résol est comprise entre 1 et 30 % en poids de la résine résorcinolique.

2. Procédé selon la revendication 1, dans lequel :

A. La quantité du premier composant est comprise entre 99 parties et 70 parties en poids ;

B. la quantité du deuxième composant est comprise entre 1 et 30 parties en poids ;

C. le pH de la résine résol est au moins 9 ; et

D. le pH de la résine résorcinolique est compris entre 6 et 9.

3. Procédé selon la revendication 1, dans lequel le donneur de méthylène est un élément choisi dans le groupe constitué par trioxanne ; hexaméthylène tétramine ; produits d'addition d'éthylènediamine et de formaldéhyde ; triformals cycliques ; oxazolidine dépourvu d'un groupe méthylol ; et composés méthylolés qui agissent comme

4. Procédé selon la revendication 2, dans lequel le donneur de méthylène est une oxazolidine avec ou sans groupe méthylol faisant partie de l'oxazolidine.

5. Procédé selon la revendication 2, dans lequel le donneur de méthylène est une méthylolurée.

6. Procédé selon la revendication 2, dans lequel le catalyseur dans le deuxième composant est un carbamate.

7. Procédé selon la revendication 1, dans lequel :

A. Le catalyseur de prise à fonction ester est un élément choisi dans le groupe constitué par un carbonate organique cyclique, une lactone et un ester d'acide carboxylique ; et

B. le carbamate est le produit de réaction de l'ammoniac avec un élément choisi dans le groupe constitué par un carbonate d'alcoylène, un carbonate de glycidol et un carbonate de résine époxy.

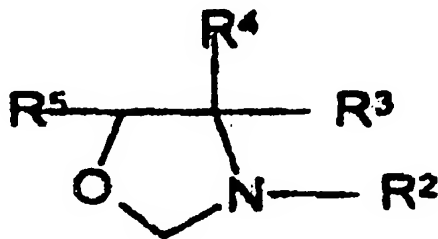
8. Procédé selon la revendication 2, dans lequel le catalyseur pour la résine résol est un catalyseur de prise à fonction ester.

9. Procédé selon la revendication 2, dans lequel le catalyseur dans le deuxième composant est un carbamate, ledit carbamate étant le produit de réaction du carbonate d'éthylène ou du carbonate de propylène avec l'ammoniac.

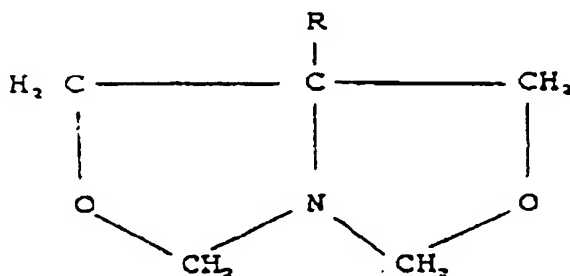
10. Procédé selon la revendication 6, dans lequel le catalyseur de type ester a de 3 à 9 atomes de carbone.

11. Procédé selon la revendication 2, dans lequel :

A. Le donneur de méthylène est un élément choisi parmi une oxazolidine représentée par la formule :



dans laquelle R² est un hydrogène, un alcoyle de 1 à 8 atomes de carbone, un hydroxyalcoyle de 1 à 8 atomes de carbone, un benzyle ou un phénylcarbamyle, et R³, R⁴ et R⁵ sont chacun un hydrogène ou un alcoyle de 1 à 8 atomes de carbone ; et



où R est hydrogène, méthyle, éthyle, n-propyle, isopropyle, méthylol, bêta-hydroxyéthyle, acétoxyméthyle ou méthoxyméthyle ; et

B. l'ester est un élément choisi dans le groupe constitué par une lactone, un carbonate organique cyclique, un ester d'acide carboxylique et des mélanges de ceux-ci.

12. Procédé selon la revendication 2, dans lequel la résine résol est le produit de condensation du phénol et du formaldéhyde.

13. Procédé selon la revendication 2, dans lequel la résine résorcinolique est un élément choisi dans le groupe constitué par le produit de condensation du résorcinol et du formaldéhyde ; et le produit de condensation du phénol, du résorcinol et du formaldéhyde contenant jusqu'à 55 parties en poids de phénol pour 50 parties de résorcinol.

14. Procédé selon la revendication 13, dans lequel la résine résorcinolique est le produit de condensation du résorcinol et du formaldéhyde.

15. Procédé selon la revendication 13, dans lequel la résine résorcinolique est le produit de condensation du résorcinol avec moins de 10 parties de phénol.

16. Procédé selon la revendication 11, dans lequel l'azote de l'oxazolidine fait partie d'un hétérocycle à cycle unique.

17. Procédé selon la revendication 11, dans lequel l'azote de l'oxazolidine est directement attaché à un premier cycle et un deuxième cycle de l'oxazolidine.

18. Procédé selon la revendication 17, dans lequel l'oxazolidine est le 1-aza-5-méthylol-3,7-dioxa-bicyclo[3.3.0]octane.

19. Procédé selon la revendication 17, dans lequel l'oxazolidine est le 1-aza-5-éthyl-3,7-dioxabicyclo[3.3.0]octane.

20. Procédé pour polymériser une résine résol phénolique monohydroxylique avec un précondensat de résine résorcinolique ayant un déficit de formaldéhyde, qui comprend le mélange de :

A. 70 à 99 parties d'un premier composant ayant un pH d'au moins 9 et comprenant une solution de résine résol phénolique monohydroxylique alcaline aqueuse stable contenant de 0,3 à 15 % sur la base du poids de la solution de résine résol d'un donneur de méthylène choisi parmi des composés qui n'ont pas de groupe méthylol et des composés qui ont un groupe méthylol ; avec

B. 1 à 30 parties d'un deuxième composant comprenant un précondensat de résine résorcinolique aqueux stable ayant un déficit de formaldéhyde et un pH de 6 à 9 et de 1 à 30 % en poids sur la base du poids de la résine résorcinolique d'un catalyseur pour la résine résol choisi parmi des catalyseurs de prise à fonction ester et de catalyseurs de type carbamate.

21. Procédé selon la revendication 20, dans lequel le donneur de méthylène est une oxazolidine.

22. Procédé selon la revendication 20, dans lequel le donneur de méthylène est une méthylolurée.

23. Composition adhésive alcaline ayant un pH d'au moins 9 et préparée en mélangeant :

A. 70 à 99 parties en poids d'un premier composant comprenant une solution de résine résol phénolique monohydroxylique alcaline aqueuse stable ayant un pH d'au moins 9 et contenant de 0,5 % à 10 %, sur la base du poids de la solution, d'un donneur de méthylène choisi parmi des composés qui n'ont pas de groupe méthylol et des composés qui ont un groupe méthylol ; et

B. 1 à 30 parties d'un deuxième composant comprenant une solution de résine résorcinolique aqueuse stable ayant un pH compris entre 6,5 et 8,5 et contenant de 5 % à 25 %, sur la base du poids de la résine, d'un catalyseur pour la résine résol, ledit catalyseur étant choisi dans le groupe constitué par un catalyseur de prise à fonction ester et un carbamate.

24. Adhésif selon la revendication 23, dans lequel le catalyseur est un catalyseur de prise à fonction ester ayant de 3 à 9 atomes de carbone, choisi dans le groupe constitué par un ester d'acide carboxylique, un carbonate organique cyclique et une lactone.

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25. Composition adhésive selon la revendication 23, dans laquelle le pH de la résine résol est au moins 10.
26. Composition selon la revendication 23, dans laquelle le donneur de formaldéhyde est une méthylolurée.
- 5 27. Composition selon la revendication 23, dans laquelle le donneur de formaldéhyde est une oxazolidine.
28. Procédé pour la production de panneaux lignocellulosiques en collant des composants lignocellulosiques dans des conditions de chaleur et de pression, dans lequel on revêt des composants lignocellulosiques d'un adhésif comprenant un mélange de :
- 10 A. 70 à 99 parties en poids d'un premier composant comprenant une solution de résine résol phénolique monohydroxylique alcaline aqueuse stable contenant de 0,3 % à 15 %, sur la base du poids de la résine résol, d'un donneur de méthylène choisi parmi des composés qui n'ont pas de groupe méthylol et des composés qui ont un groupe méthylol ; et
- 15 B. 1 à 30 parties d'un deuxième composant comprenant une résine résorcinolique polymérisable contenant de 1 % à 30 %, sur la base du poids de la résine résorcinolique, d'un catalyseur pour la résine résol, ledit catalyseur étant choisi dans le groupe constitué par un catalyseur à fonction ester et un carbamate qui est le produit de réaction d'un carbonate choisi dans le groupe constitué par des carbonates d'alcoylène, de glycidol et de résine époxy avec l'ammoniac.
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